AMENDMENTS TO THE CLAIMS:

This listing of claims will replace all prior versions and listings of claims in the application:

- 1. (Original) A method for producing an alcohol and/or a ketone, wherein a raw material containing at least one alkene is contacted and reacted with an oxide catalyst in the presence of steam in a gas phase to produce an alcohol and/or a ketone corresponding to said alkene(s), which comprises satisfying the following requirements of (a) to (c):
 - (a) said oxide catalyst contains an oxide(s) of molybdenum and/or tin;
- (b) said reaction is carried out under a condition where molecular oxygen is not fed and by the use of a system wherein said catalyst is circulated between a fluid bed reactor and a regenerator; and
 - (c) a stripper is provided on the way from said regenerator to said reactor.
- 2. (Original) The method according to claim 1, wherein a stripper is further provided on the way from said reactor to said regenerator.
- 3. (Original) The method according to claim 1 or 2, wherein said alkene(s) is 1-butene and/or 2-butene.
- 4. (Currently amended) The method according to any one of claims $\frac{1}{1}$ [[to 3]] or 2, wherein the atomic ratio X of molybdenum to the sum of tin and molybdenum contained in said oxide catalyst ((Mo/ (Sn + Mo) where Mo is the number of molybdenum atoms in said oxide catalyst and Sn is the number of tin atoms in said oxide catalyst) is in the range of $0 \le X < 0.50$.

- 5. (Currently amended) The method according to any one of claims claim 1 [[to 3]]or 2, wherein the atomic ratio X of molybdenum to the sum of tin and molybdenum contained in said oxide catalyst ((Mo/ (Sn + Mo) where Mo is the number of molybdenum atoms in said oxide catalyst and Sn is the number of tin atoms in said oxide catalyst) is in the range of $0.01 \le X < 0.24$.
- 6. (New) The method according to claim 3, wherein the atomic ratio X of molybdenum to the sum of tin and molybdenum contained in said oxide catalyst
 ((Mo/ (Sn + Mo) where Mo is the number of molybdenum atoms in said oxide catalyst and Sn is the number of tin atoms in said oxide catalyst) is in the range of 0 ≤ X < 0.50.
- 7. (New) The method according to claim 3, wherein the atomic ratio X of molybdenum to the sum of tin and molybdenum contained in said oxide catalyst ((Mo/(Sn + Mo))) where Mo is the number of molybdenum atoms in said oxide catalyst and Sn is the number of tin atoms in said oxide catalyst) is in the range of $0.01 \le X < 0.24$.